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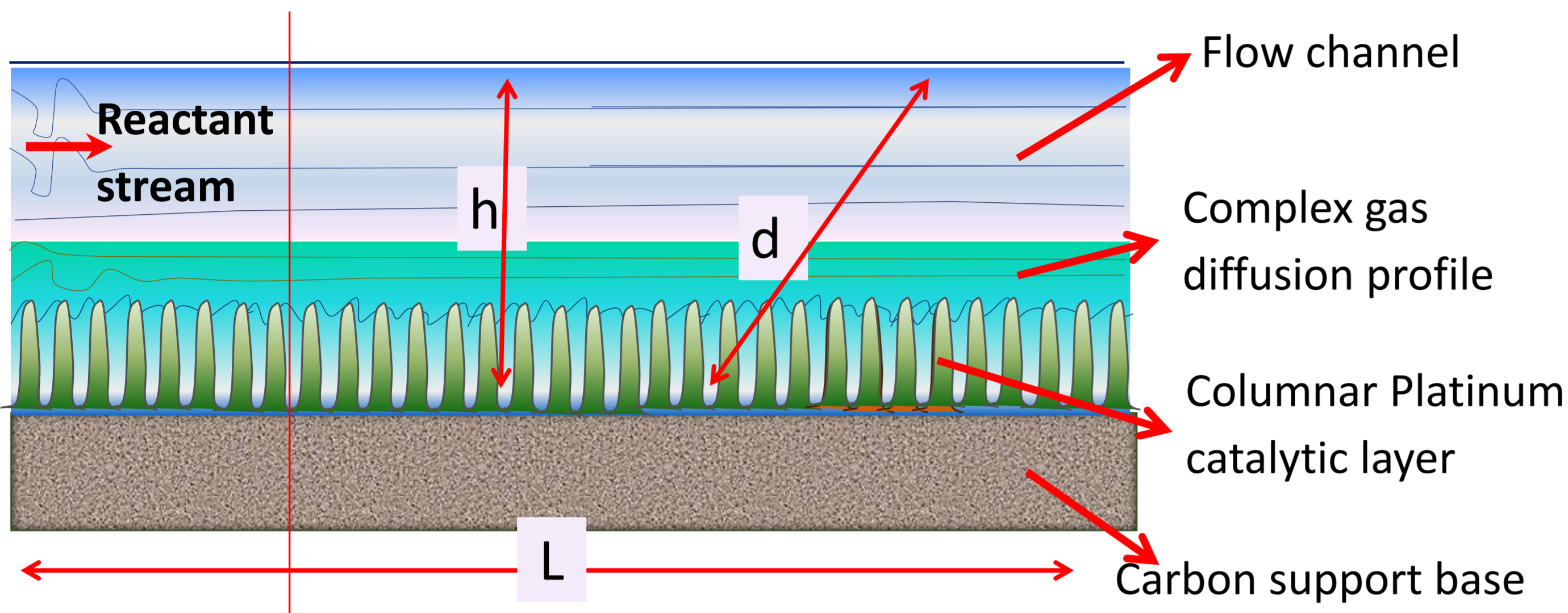
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Summary

Dimensionless Operating Numbers were obtained for long time hydrogen/oxygen PEMFC performance employing mass, charge and linear momentum transport equations.

Surface roughness for long time operating electrocatalysts developed as platinum columnar anode and cathode after 6 months at 1 A cm⁻² and loads larger than 1 mg cm⁻².

Current and potential distributions were developed modelling the columnar catalysts using trochoid curvilinear profiles with the help of *ex situ* STM images. This modelling allows the reduction of variables in the differential equations and permits an exact resolution.



Scheme 1.- Gas reactant flow stream along a 2 D channel in a PEMFC at laminar convective diffusion semi-infinite regimes. Thin catalytic layer of columnar platinum.

2 D Velocity Profile into t -dependent

$$v_x \left(\frac{\partial v_x}{\partial x} \right) + v_y \left(\frac{\partial v_x}{\partial y} \right) = v \left(\frac{\partial^2 v_x}{\partial y^2} \right) + v \left(\frac{\partial^2 v_x}{\partial x^2} \right)$$

$$v_x \left(\frac{\partial v_x}{\partial t} \right) [1 - \log(1 - \lambda \cos t)] =$$

$$v \left(\frac{\partial^2 v_x}{\partial t^2} \right) \left(\frac{\sec t + c \sec t}{\lambda} - 1 - ctgt \right)$$

Asymptotic solutions

$$v_x \cong U^o t$$

$$v_y \cong \frac{U^o \lambda t^2}{2(1-\lambda)}$$

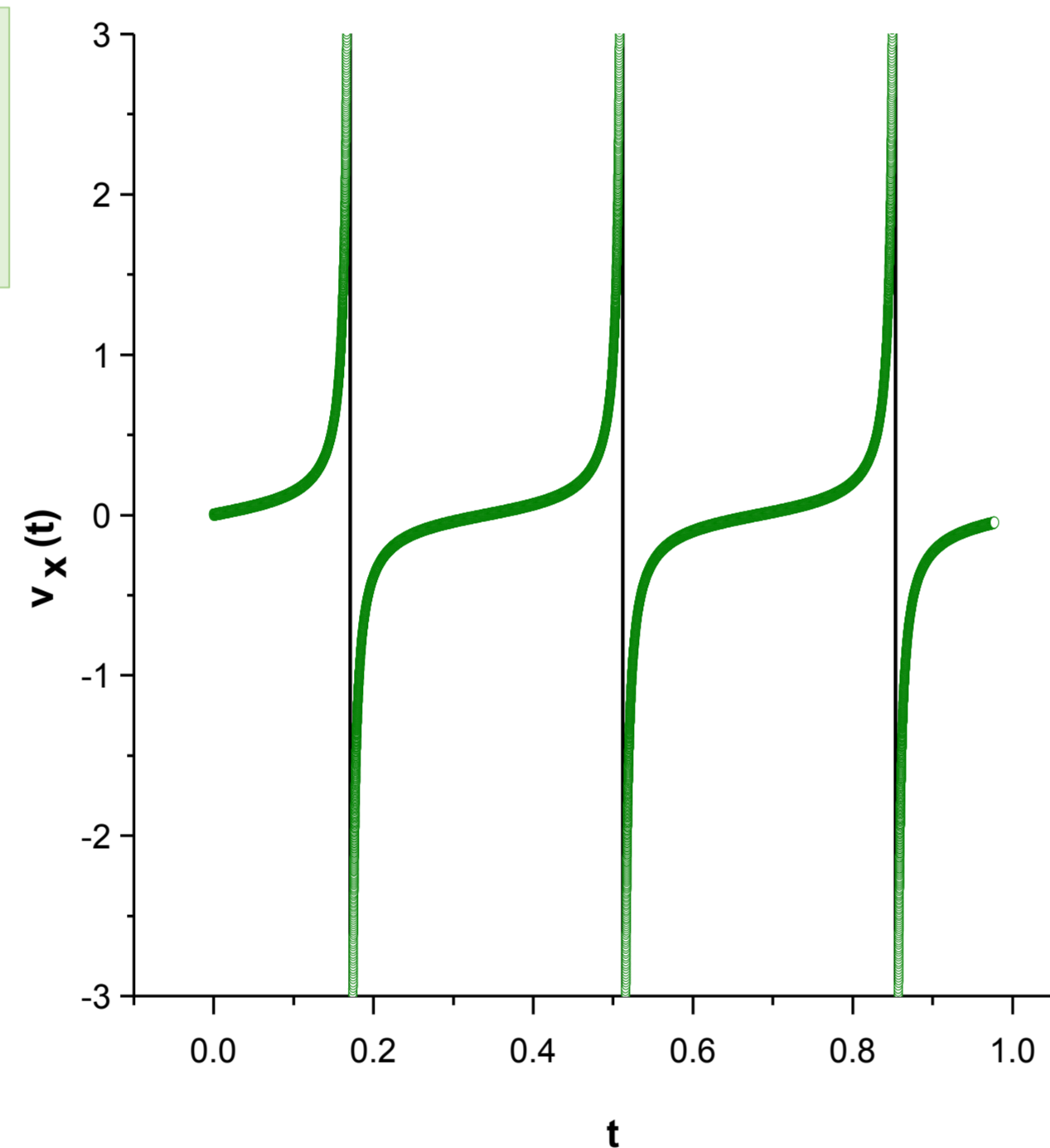


Figure 4.- Repetitive tangential velocity profile along the parametric columnar platinum.

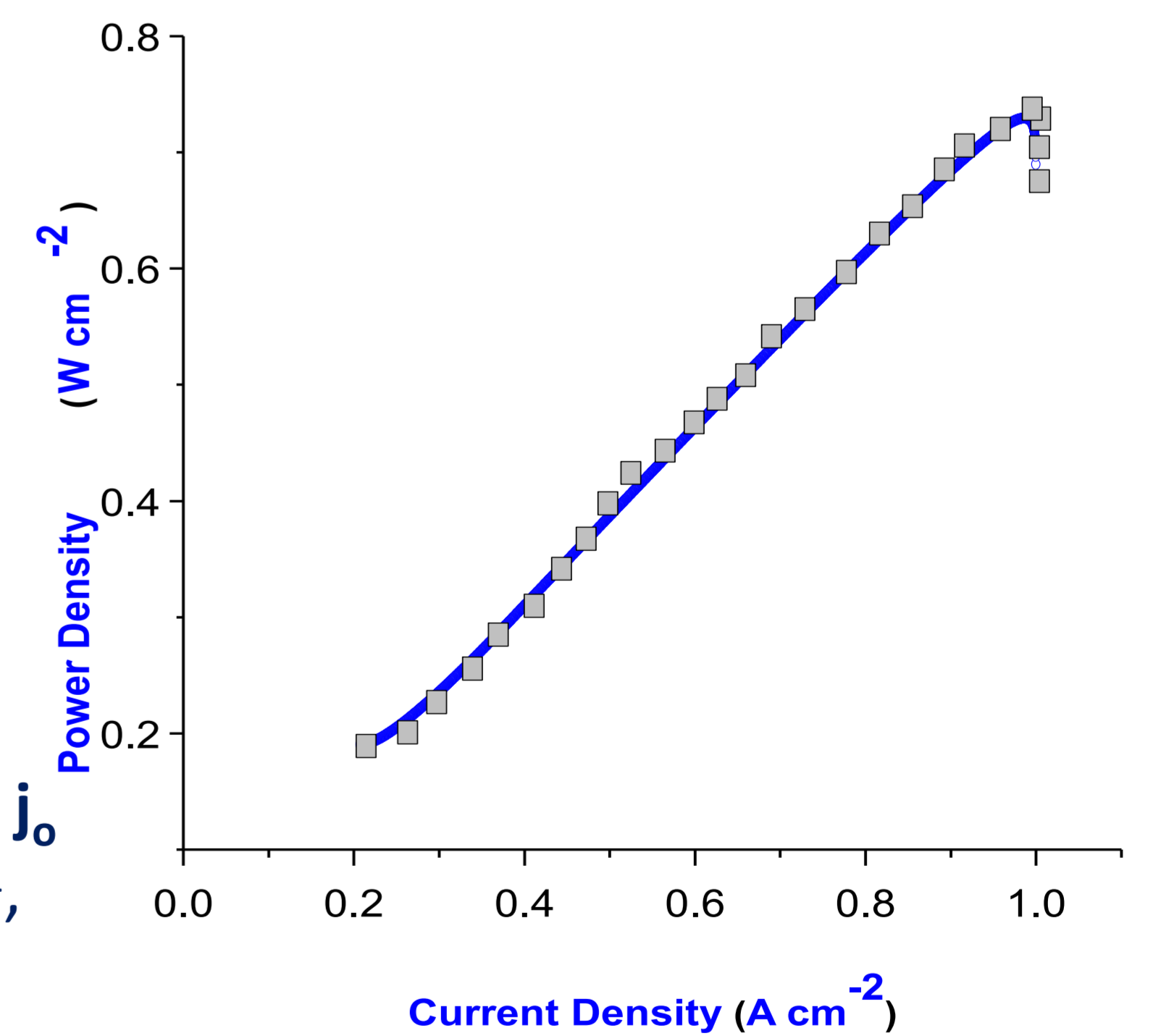
Polarization Curves

$$v_x \left(\frac{\partial C}{\partial x} \right) + v_y \left(\frac{\partial C}{\partial y} \right) = D \left(\frac{\partial^2 C}{\partial y^2} \right) \pm \frac{\partial}{\partial x} \left(\frac{j}{nF} \right)$$

$$\eta(t) = b \ln \left(\frac{j_o}{nFDC^o} \right) - \frac{b \alpha \lambda (3(\lambda t^2 - 2) \sin t - t^3 + 6t \cos t)}{6(\lambda - 1)D / U^o} + b \ln \left[\frac{0.42 t \Gamma \left(0.33, -\frac{\alpha \lambda U^o t^3}{2D} \right)}{\sqrt[3]{-\frac{\alpha \lambda U^o t^3}{2D}}} + \frac{0.81}{\sqrt[3]{\frac{\alpha \lambda U^o}{D}}} \right]$$

$$j(t) = nFD \frac{dC(t)}{dt} = nFD \exp \left(\frac{\alpha \lambda (3(\lambda t^2 - 2) \sin t - t^3 + 6t \cos t)}{6(\lambda - 1)D / U^o} \right)$$

Figure 5.- Power Density vs. Current Density. $j_o = 0.75 \text{ A cm}^{-2}$, $v = 0.01 \text{ cm}^2 \text{ s}^{-1}$, $U^o = 0.16 \text{ cm s}^{-1}$, $b = 0.03 \text{ V dec}^{-1}$, $n = 2$, $D = 0.05 \text{ cm}^2 \text{ s}^{-1}$.



Dimensionless Numbers

The Wagner (**Wa**), Damkoehler (**Da**), Schmidt (**Sc**) and Graetz (**Gz**) numbers define the electrochemical reactor dimensionless equation:

$$Da(T) = 3(Da_i) \frac{Sc^{1/6}}{Gz^{1/2}} w \sqrt{\alpha(T - \lambda \sin T)} e^{-\Phi(T)} e^{-J(T)/Wa}$$

Being Da_i the onset Damkoehler number and w the characteristic length on the PEMFC. $\Phi(T)$ and $J(T)$ are the potential and current distributions.

$$Da = \frac{j_o e^{-\alpha f(E-E_{j=0})}}{nFDC^o / \delta}$$

$$Gz = \frac{D_h}{L} \text{Re} \text{Sc}$$

$$Wa = \frac{b / j_o}{R_\Omega}$$

$$Da_i = \frac{j_{o,c} d}{nFDC^o}$$

$$w \equiv \frac{\sqrt{L(2h - D_h)}}{h \sqrt{D_h}}$$

Results

Figure 1.- Initial cyclic voltammetry of anodic platinum (blue lines) and final profile after 6 months of continuous operation (red lines) at $v = 0.10 \text{ Vs}^{-1}$ in 0.50 M sulphuric acid.

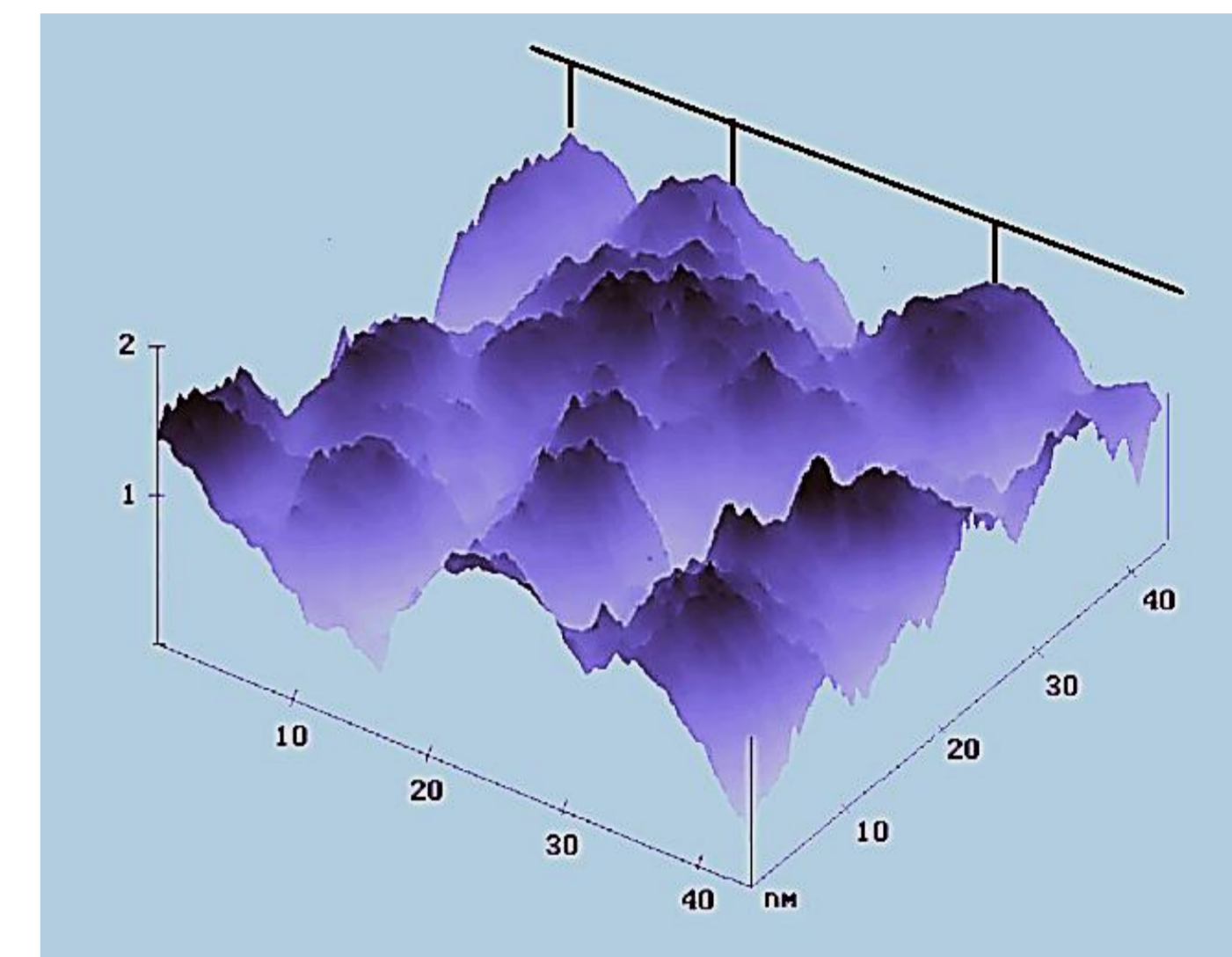
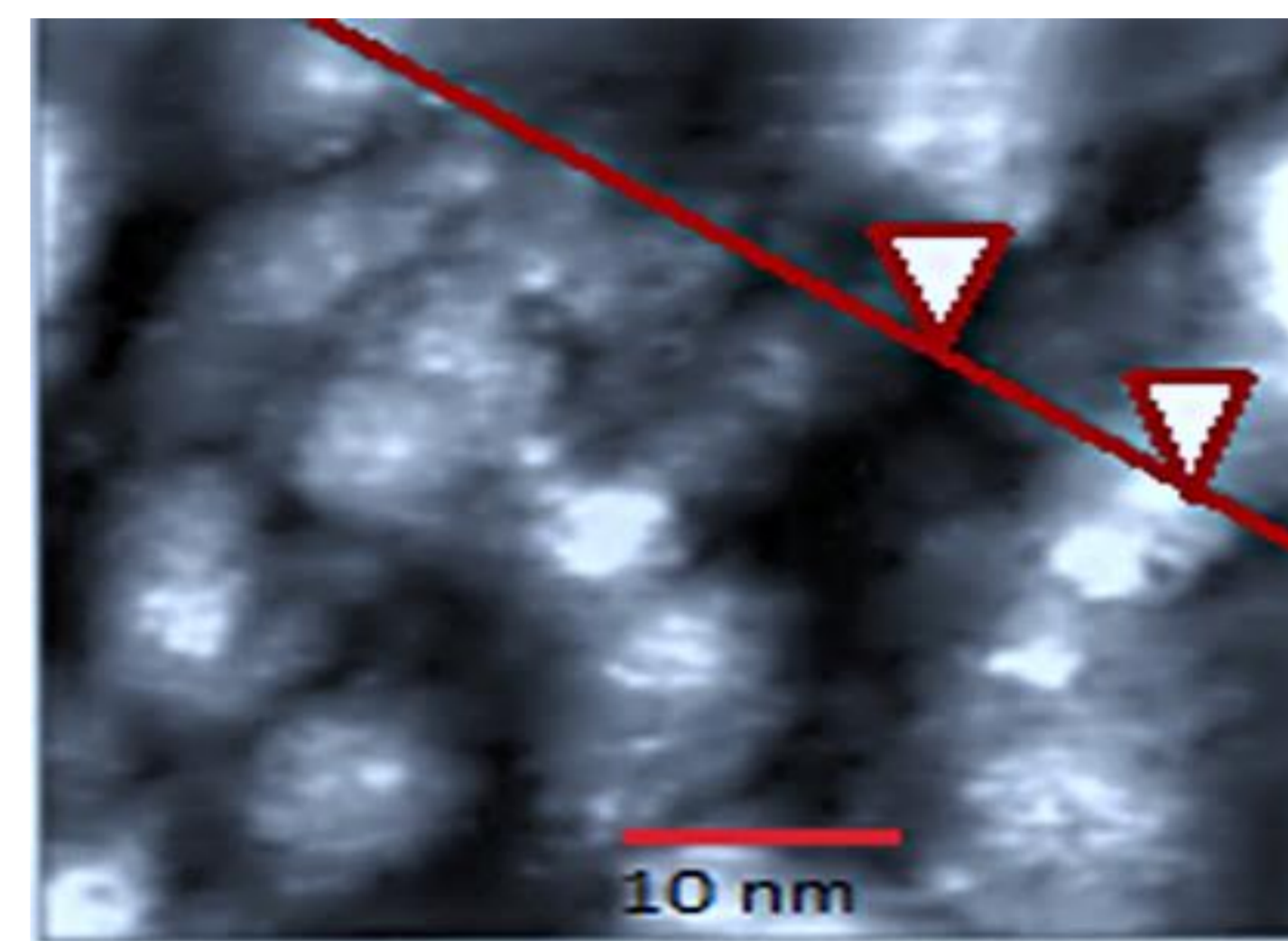
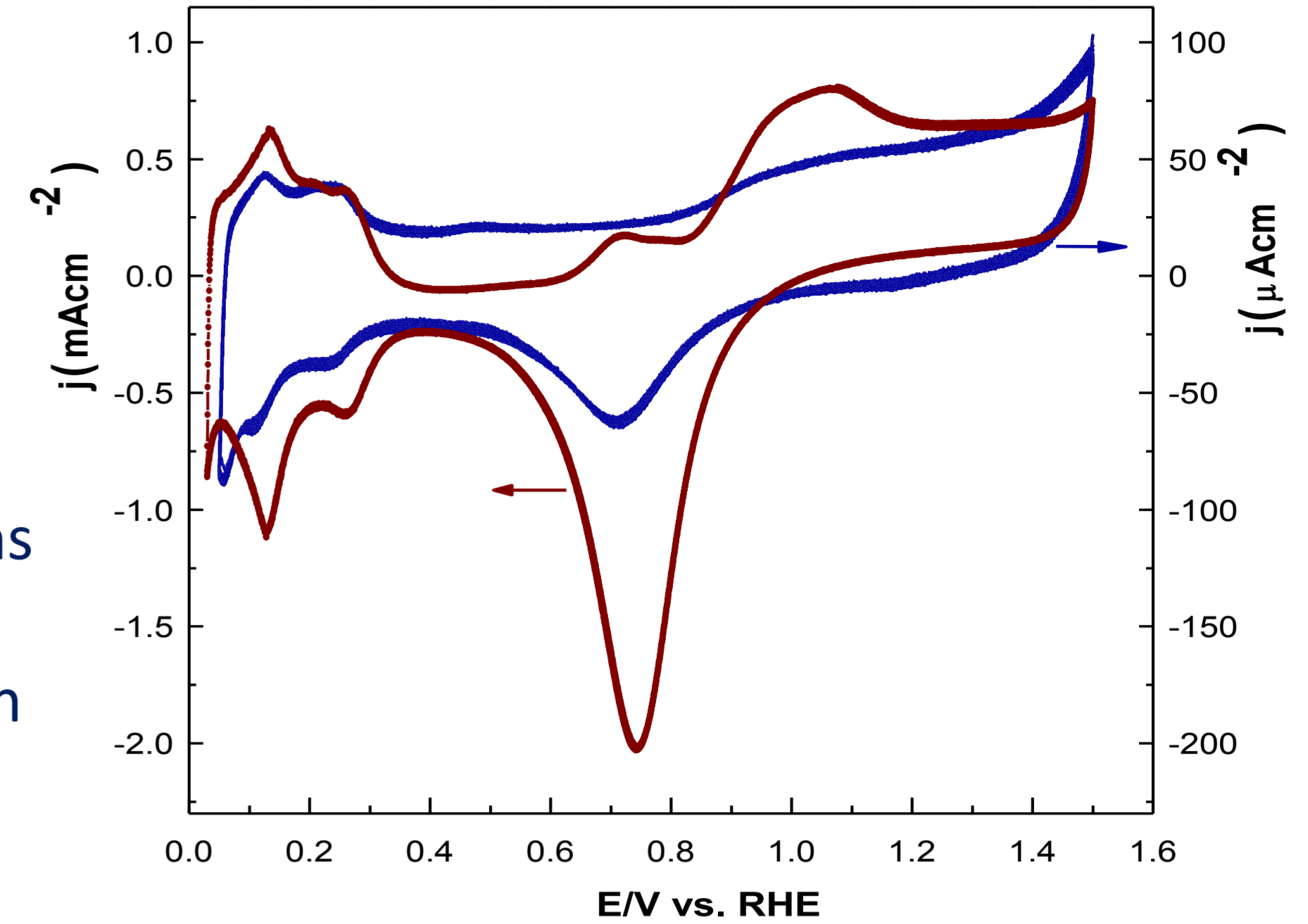


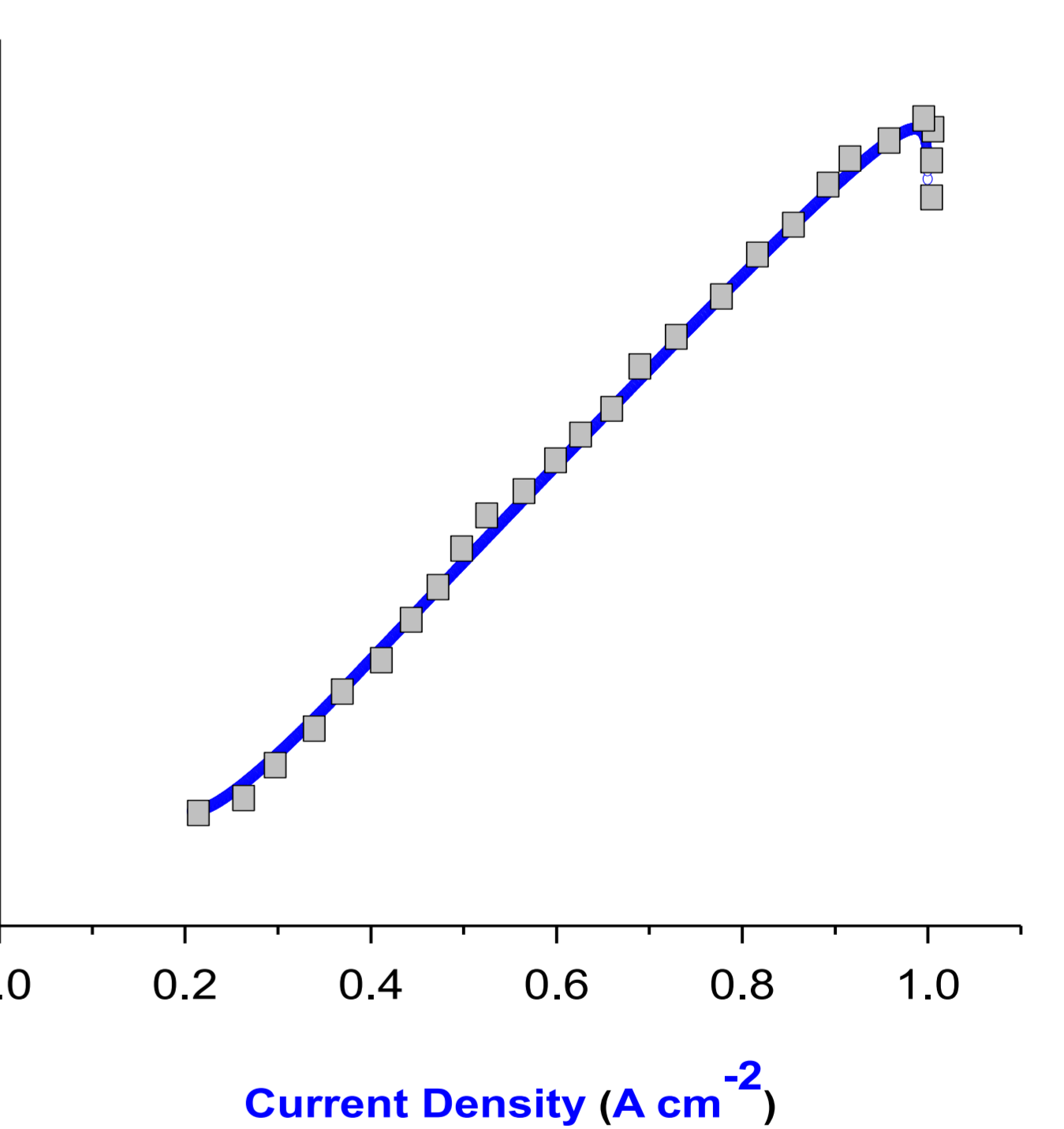
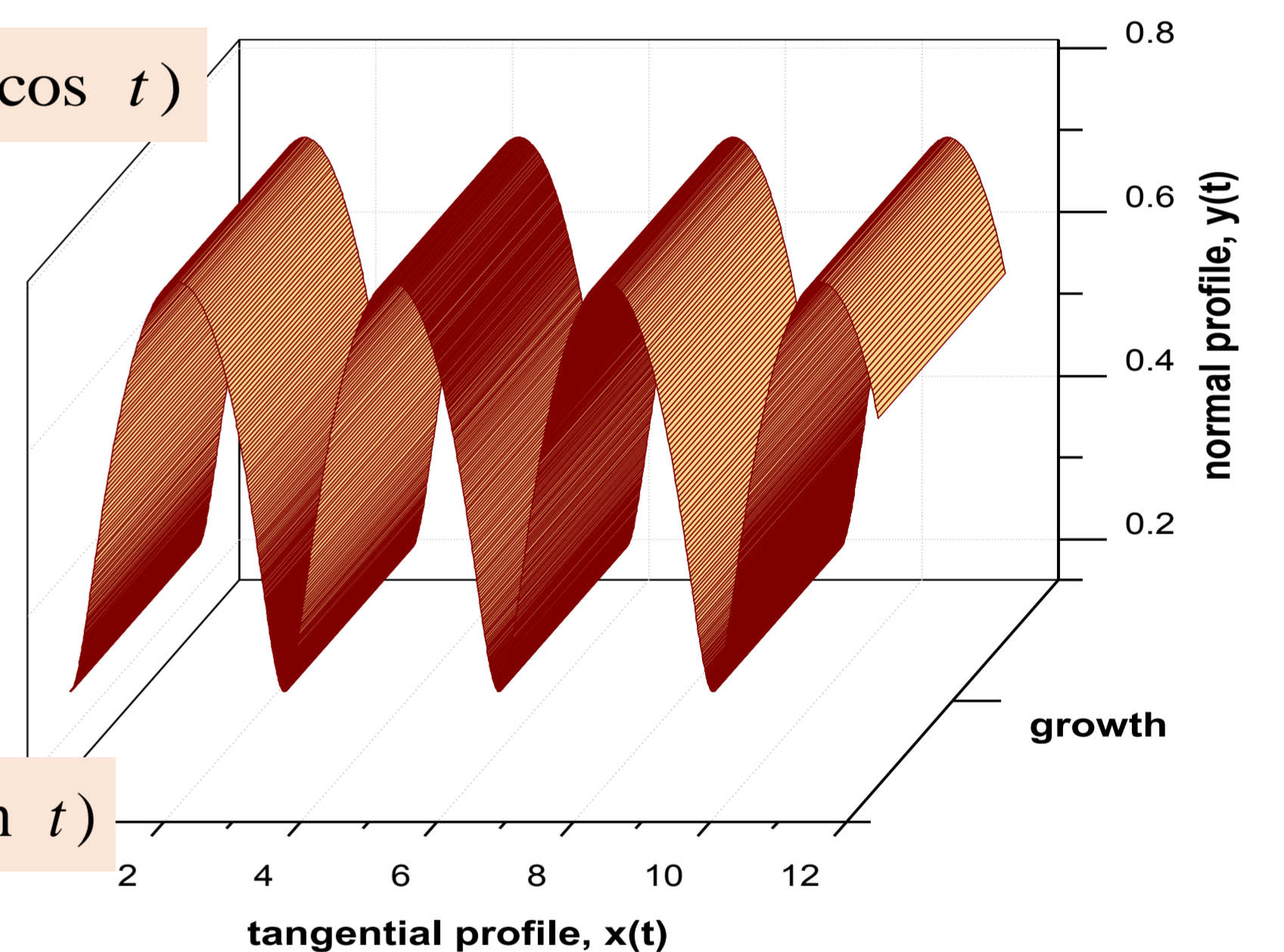
Figure 2.- *ex situ* STM images -left panel- cross section mode, tasks define the inter-column distance. -right panel- topographic mode after 6 months of operation of the hydrogen/oxygen PEMFC.

columnar platinum structure

$$y(t) = \alpha (1 - \lambda \cos t)$$

Figure 3.- Parametric periodic platinum columnar surface (trochoid) path $\lambda = 0.5$ and radius $\alpha = 0.5$.

$$x(t) = \alpha (t - \lambda \sin t)$$



$Gz_{t,ohm}(T)$

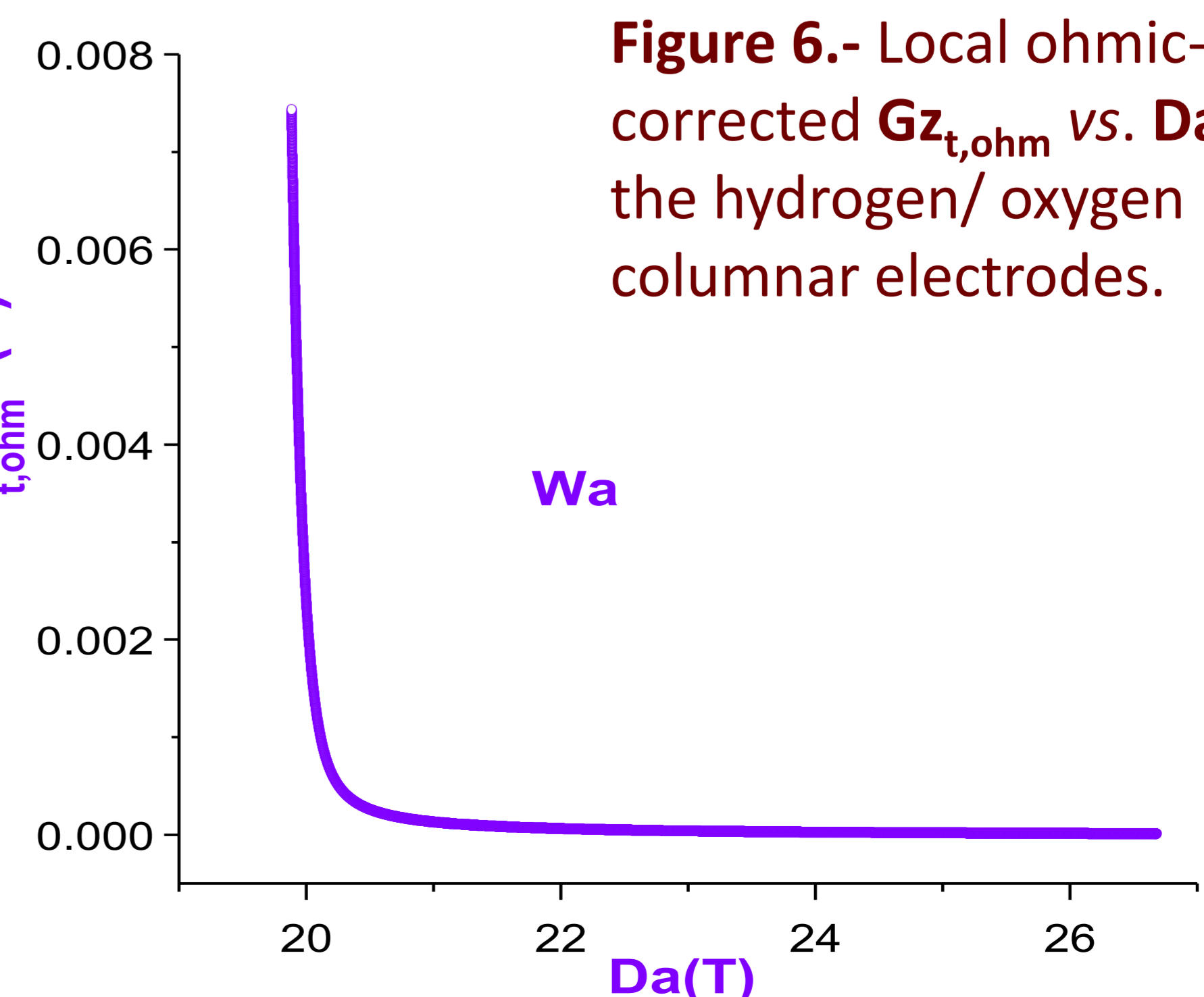


Figure 6.- Local ohmic-drop corrected $Gz_{t,ohm}$ vs. $Da(T)$ for the hydrogen/oxygen PEMFC at columnar electrodes.